

# Effect of Saturating the Electrolyte with Oxygen on the Activity for the Oxygen Evolution Reaction

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## Supporting Information

### INTRODUCTION

With the increased interest in the electrochemical conversion of renewable electricity, water, and carbon dioxide to fuels, there is an ever-growing number of papers reporting new electrocatalysts for the oxygen evolution reaction (OER).<sup>1–5</sup> The OER is the anode reaction in the electrolysis of water and CO<sub>2</sub> and a major source of efficiency loss, because of its high overpotential.<sup>6</sup> To meaningfully compare the activity of the many new materials that are currently synthesized and tested, it is important that the research community agrees on proper standardization, benchmarking, and best practices.<sup>7,8</sup>

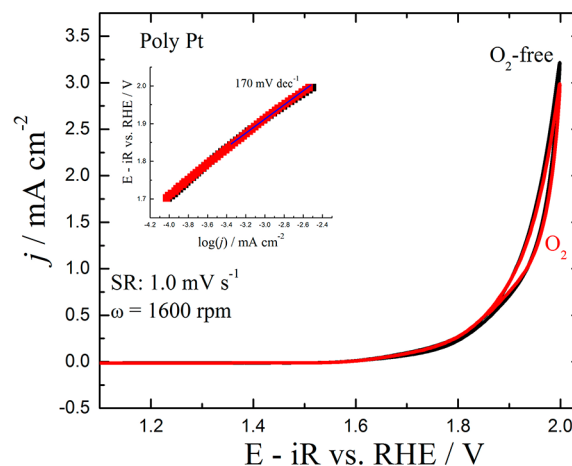
Several papers reporting on the activity of OER state that it is necessary to saturate the electrolyte with oxygen gas before measurement, in order for the electrode “to reach its rest potential” or “to fix the equilibrium potential”,<sup>2,9–14</sup> and saturating the solution with oxygen seems to have become an often-employed practice (see, e.g., refs 15–18). A recent paper claimed that oxygen in the electrolyte may reduce the OER activity on nickel (supported on graphene) and change the Tafel slope via a van der Waals-type interaction of molecular oxygen with the active site, hampering access by hydroxide ions.<sup>11</sup> The argument to fix the equilibrium potential is based on the idea that, in the absence of oxygen, the driving force for oxygen evolution should be higher than in its presence. However, at a given electrode potential, the rate of oxygen evolution itself must be independent of whether O<sub>2</sub> is present in solution or not. What potentially changes in the presence of oxygen is the rate of the back reaction, i.e., the oxygen reduction reaction (ORR), and therefore the *net* production rate of oxygen may be dependent on whether O<sub>2</sub> is present or not. This could play a role for a reversible reaction near its equilibrium potential, but it should be irrelevant for an irreversible reaction such as OER (ORR rates can safely be neglected above 1.3 V). The rate of an electrode reaction at a given applied potential is more accurately measured in the absence of the product, regardless of whether, under the experimental conditions, the equilibrium potential is well-defined or not. This also implies that the overpotential, when defined as the difference between the applied potential and the equilibrium potential, is not well-defined in the absence of oxygen in solution, but this has no (theoretical) effect on the rate of the OER at a given applied potential. Of course, close to equilibrium, it may still be necessary to correct for any current due to the back reaction if one wants to know the rate of the forward reaction only. The notion that the presence of O<sub>2</sub> in solution may have an effect on the state of the surface (and thereby influence its chemistry and “rest potential”) has been studied for platinum electrodes.<sup>19,20</sup> It was found that O<sub>2</sub> in

solution may indeed have an effect on the activity and stability of platinum electrodes, but apparently only under potential cycling conditions, or at relatively negative potentials, suggesting that oxygen reduction may play a role. Kongkanand and Ziegelbauer concluded that the effect of O<sub>2</sub> in solution on the oxide coverage on platinum is negligible.<sup>19</sup>

To clarify the experimental role of oxygen saturation of the electrolyte on OER activity, we decided to study the effect of electrolyte oxygen on the OER on Pt and Ni-oxyhydroxide electrodes. In this Viewpoint, we show that (i) oxygen dissolved in the electrolyte has no significant effect on the OER activity (at least not on Pt-oxide and Ni-oxyhydroxide surfaces) and (ii) in the standardization of best practices for OER studies, care should be taken in employing a proper (placement of the) reference electrode, and in taking measures that small oxygen bubbles are efficiently removed from the electrocatalyst surface (for instance, by rotation).

### EXPERIMENTAL RESULTS

Although platinum is not the best catalyst for the OER, we use it in this work as a model system to provide insight into the effect of different parameters. Figure 1 shows the current–



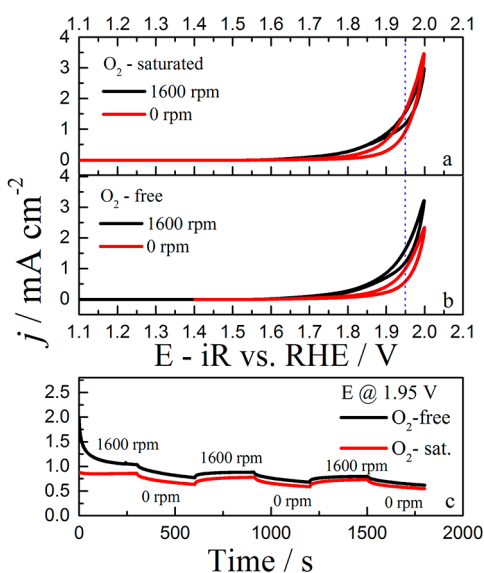
**Figure 1.** Cyclic voltammetry for polycrystalline Pt in pH 13 in the region of oxygen evolution reaction under rotation of the electrode at 1600 rpm. Scan rate = 1.0 mV s<sup>-1</sup>. Measurements were performed using an Ag/AgCl reference electrode. [Legend: red line denotes electrolyte saturated with O<sub>2</sub>; black line denotes electrolyte saturated with Ar, with no O<sub>2</sub> present.]

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potential profiles obtained during water oxidation catalyzed by polycrystalline Pt at pH 13, with the electrolyte saturated with O<sub>2</sub> (red line) and the electrolyte obtained by removing oxygen from the solution (black line), under rotation of the electrode at 1600 rpm and at a scan rate of 1.0 mV s<sup>-1</sup>. The onset potential of the OER is ~1.57 V vs RHE and no significant difference are observed between the O<sub>2</sub>-saturated solutions and the O<sub>2</sub>-free solutions. Under both conditions, the *iR*-corrected Tafel plots (see inset in Figure 1) show a similar slope of 170 mV dec<sup>-1</sup>, in agreement with the literature.<sup>21</sup> The same insensitivity to O<sub>2</sub> saturation was observed in acidic solution (result not shown).

Figure 2 compares the effect of the rotation for the same curves showed in Figure 1. There is a clear effect of the



**Figure 2.** Cyclic voltammetry for polycrystalline Pt in pH 13 in the region of oxygen evolution reaction. (a) O<sub>2</sub>-saturated and (b) O<sub>2</sub>-free solution at 1600 rpm and without rotation. Scan rate = 1.0 mV s<sup>-1</sup>, using a Ag/AgCl reference electrode. (c) Chronoamperometry curves at E = 1.95 V vs RHE. [Legend: red line represents the presence of O<sub>2</sub>; black line represents the absence of O<sub>2</sub>.]

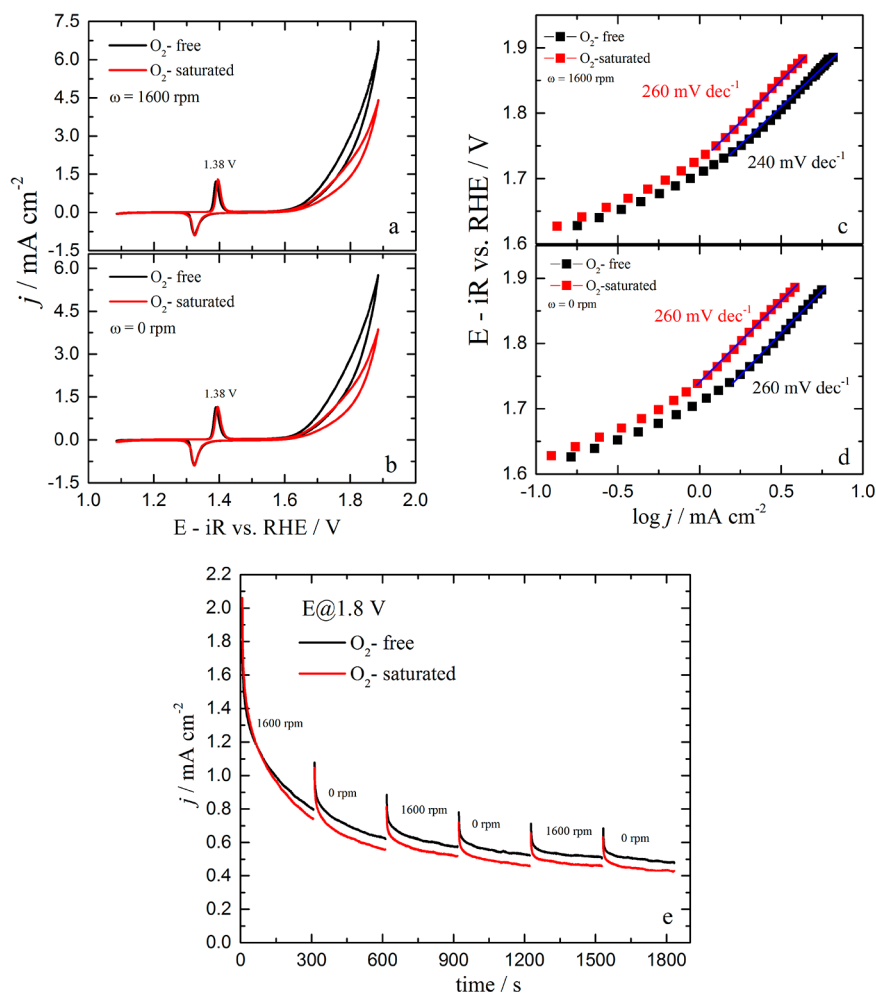
rotation rate of the RDE, comparing OER current–voltage curves and chronoamperometry measurements with and without rotation ( $\omega = 1600$  and 0 rpm, respectively). Figures 2a and 2b show that, in the absence of rotation, the onset of OER is delayed, both for the O<sub>2</sub>-saturated and O<sub>2</sub>-free solutions. We ascribe this observation to the more-efficient removal of oxygen bubbles from the electrode in the presence of rotation. However, at higher potentials, the comparison is more difficult to rationalize, because, in the O<sub>2</sub>-saturated solution, the absence of rotation leads to a higher current. We note that voltammetric OER rates are generally not perfectly reproducible when the electrode is not rotated. To add to the complication of comparing these curves, the effects are dependent on the scan rate. At 10 mV s<sup>-1</sup>, we observe no difference between rotation and no rotation for both electrolytes, whereas, at 50 mV s<sup>-1</sup>, the OER current is higher in a stagnant O<sub>2</sub>-free solution (these data are shown in Figure S1 in the Supporting Information). To eliminate this effect of scan rate, we also performed chronoamperometry experiments at a fixed potential of 1.95 V (vs RHE). Figure 2c compares these experiments for O<sub>2</sub>-saturated (red curve) and O<sub>2</sub>-free

solutions (black curve). In the beginning of the experiment, when both electrodes are rotated, the O<sub>2</sub>-free solution gives a higher OER current than the O<sub>2</sub>-saturated solution. We attribute this observation to the more-facile nucleation of oxygen bubbles on the platinum electrode in an O<sub>2</sub>-saturated solution, thereby blocking the catalytic surface. If rotation is stopped, the OER activity decreases for both electrolytes, and once rotation is started again, the activity increases again. This clearly shows that there is an important effect of rotation, which we tentatively attribute to the enhanced removal of bubbles in the presence of rotation. It is also observed that, at longer times, the OER activities in O<sub>2</sub>-saturated and (initially) O<sub>2</sub>-free solutions approach each other.

We note that, in comparing the OER activities in O<sub>2</sub>-saturated and O<sub>2</sub>-free electrolytes, it is important to use an oxygen-insensitive reference electrode and to keep oxygen rigorously away from the reference electrode. When performing the experiment using an internal hydrogen reference electrode, we noted that, in an O<sub>2</sub>-saturated solution, the onset potential for OER is substantially lower than that observed in the absence of oxygen. The reason for this turned out to be a shift in the potential of the hydrogen reference electrode, whose potential now becomes a mixed potential that is determined by hydrogen oxidation and oxygen reduction. The effect is especially significant in alkaline media, where the kinetics of the hydrogen oxidation and hydrogen evolution on platinum are comparatively slow and, hence, more sensitive to spurious side reactions. In any case, we recommend using a Hg/HgO or Ag/AgCl reference electrode for OER experiments in alkaline media, although caution should be taken with the latter as Cl<sup>-</sup> ions during long-term measurements can leach out from the reference electrode compartment and diffuse to the working electrode, possibly influencing the result of the electrochemical reaction. Another issue related to the use of the Ag/AgCl reference electrode in high pH is that Ag<sub>2</sub>O or AgOH will be formed and the electrode potential will be that of a mixed Ag/AgCl/Ag<sub>2</sub>O electrode. In addition, the presence of oxygen in the electrolyte is expected to enhance the dissolution of a platinum counter electrode.<sup>19,20</sup> While this is less of an issue for OER studies on the electrode materials used in this paper, it is of concern when studying electrocatalytic reactions on working electrodes sensitive to small amounts of platinum.<sup>8</sup>

The effect of dissolved oxygen electrolyte toward OER was also investigated using an NiOOH-based electrocatalyst, chosen for its high activity and stability in alkaline media.<sup>4,22–24</sup> We performed our measurements in Fe-free electrolyte, since Boettcher et al.<sup>13</sup> have demonstrated that even unintentional Fe impurities (at the parts per billion (ppb) level) in the stock electrolyte are sufficient to enhance the performance of NiOOH.

Figures 3a and 3b show the 10th scan obtained at a rate of 10.0 mV s<sup>-1</sup> in the presence and absence of oxygen in the solution under rotation (1600 rpm) and under stationary conditions, respectively, for freshly prepared NiOOH electrocatalysts. Both voltammograms show the Ni(OH)<sub>2</sub>/NiOOH (Ni<sup>II</sup>/Ni<sup>III</sup>) redox transition in the potential region of 1.3–1.4 V vs RHE. The potential at which this redox transition occurs is not dependent on the presence of O<sub>2</sub> in solution (a Hg/HgO electrode was used as a reference electrode). However, we note that, when using an internal RHE as a reference electrode, the redox peak shifted by ca. 0.1 V to more-negative potential in the presence of oxygen in the solution (see Figure



**Figure 3.** Cyclic voltammetry for NiOOH at pH 13 in the region of oxygen evolution reaction (a) under rotation of the electrode at 1600 rpm and (b) without rotation, respectively, and in the presence and absence of  $\text{O}_2$  in solution. (c) and (d) Corresponding Tafel plots for the cyclic voltammograms shown in panels (a) and (b), respectively. (e) Chronoamperometry curves at  $E = 1.8$  V. Scan rate =  $10.0 \text{ mV s}^{-1}$ . Measurements were performed using Hg/HgO reference electrode. [Legend: red line represents the presence of  $\text{O}_2$ ; black line represents the absence of  $\text{O}_2$ .]

S2 in the Supporting Information), because of the above-mentioned problem of the shift of the reference electrode potential.

An effect of the presence of oxygen was observed in the potential region where the oxygen evolution occurs ( $E > 1.6$  V vs RHE). Figures 3a and 3b compare the OER curves in the absence and presence of oxygen at 1600 and 0 rpm, respectively. The results show that the OER activity becomes slightly lower by saturating the solution with  $\text{O}_2$ . The Tafel slopes of the anodic scan for NiOOH at 1600 rpm (Figure 3c), in the presence and absence of oxygen, show values of 260 and  $240 \text{ mV dec}^{-1}$ , respectively. For NiOOH, in the absence of electrode rotation (Figure 3d), the currents are generally lower than in the presence of rotation (compare Figures 3a and 3b) but the Tafel slopes are similar. The results show that the highest OER activity is obtained in an  $\text{O}_2$ -free electrolyte under rotation of the electrode. The difference with the activity in an  $\text{O}_2$ -saturated electrode in the absence of rotation can be almost a factor of 2.

Figure 3c displays the current density versus time curves obtained at 1.8 V vs RHE for the NiOOH electrocatalyst. The results are similar to those obtained for polycrystalline Pt (see Figure 2c): an increase in the current density is observed when

the electrode is rotated and when oxygen is removed from the electrolyte.

It is known that nickel hydroxides can deactivate during long-term measurements. In order to ensure optimal activity of the materials, for each experiment, we performed a new Ni(OH)<sub>2</sub> film deposition. The electrodes were cycled until the cyclic voltammogram was stable. The results shown in Figure S3 in the Supporting Information confirm that, without rotation, and in  $\text{O}_2$ -free electrolyte, the deactivation of NiOOH is faster. When the electrolyte is saturated with  $\text{O}_2$ , the cyclic voltammograms overlap, suggesting good stability of the electrocatalyst surface; however, the curves obtained at rotations of  $<1600$  rpm (Figure S3b in the Supporting Information) and  $\text{O}_2$ -free electrolyte showed a slower decline, indicating good activity and stability of the electrode under these conditions.

## DISCUSSION AND CONCLUSION

The results presented in the previous section show that the presence of oxygen in the electrolyte has no (or a negative) effect on the activity of the oxygen evolution reaction. This exact origin of this negative effect is not entirely clear and may be due to changes in the state of the surface or a consequence of the formation of small bubbles accumulating on the

electrode surface.<sup>25–28</sup> In principle, the presence of oxygen in the electrolyte could lead to enhanced bubble formation, since the critical concentration to reach supersaturation is reached earlier, although, practically, the critical concentration may be very much higher than the saturation concentration, such that the effect may be small.<sup>29</sup> Bubbles can be removed by rotating the electrode or by stirring of the electrolyte when the electrode cannot be rotated. Comparing our results for Pt and NiOOH electrodes, the effect seems to be more severe for the NiOOH electrode, which we tentatively ascribe to the more porous structure of the NiOOH film.<sup>28</sup> Therefore, saturating the electrolyte with O<sub>2</sub> may resemble the conditions in a real electrolyzer more closely.

In addition, an important secondary issue that must be considered during OER measurements is related to the use of the reference electrode. In the presence of oxygen, one must take care to avoid having a mixed reference potential, and confirm the oxygen insensitivity of the reference electrode used.

## ■ EXPERIMENTAL SECTION

### Experimental Conditions, Electrodes, and Reactants.

Electrochemical measurements were performed at room temperature (20 ± 1 °C) with an Autolab PGSTAT12 system, using a single-compartment three-electrode cell that was composed of fluorinated ethylene propylene (FEP). The cell and all glassware used were rigorously cleaned before starting the experiments by storing overnight in concentrated H<sub>2</sub>SO<sub>4</sub> to remove metals and organic contaminants. Before use, it was rinsed and boiled five times in water to ensure the cleanliness of the system. All water used for cleaning and preparing electrolyte solutions was demineralized and ultrafiltered by a Millipore Milli-Q system (resistivity of >18.2 MΩ, TOC < 5 ppb).

The chemicals used in this work were of ultrahigh purity: Ni(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O (Aldrich trace metal basis, 99.999%), H<sub>2</sub>SO<sub>4</sub> (Aldrich, 98%), and NaOH (Aldrich, 30% solution in H<sub>2</sub>O, TraceSelect for trace analysis).

For the OER measurements, high-area Pt and Au counter electrodes were used (the latter for measurements using NiOOH as a catalyst). A commercial and self-contained RHE (Gaskatel, Hydroflex), consisting of polytetrafluoroethylene (PTFE), a silver–silver chloride (Ag/AgCl), and a mercury–mercury oxide (Hg/HgO), was used as a reference electrode.

The working electrodes were a polycrystalline Pt rotating disk electrode, or a Ni film deposited on Au rotating-disk electrode (RDE) ( $\phi = 0.196 \text{ cm}^2$ ). Before measurements, the RDE electrode was first polished with 0.3 and 0.05 μm alumina paste (Buehler, Ltd.). Subsequently, the electrode was sonicated for 5 min to remove polishing particles. All experiments were performed at 0 or 1600 rpm (unless otherwise stated).

Nickel was plated on the polycrystalline gold electrode by galvanostatic electrodeposition from 5 mM Ni(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O solution, using 0.1 M NaClO<sub>4</sub> as a supporting electrolyte. The deposition was carried out by applying a cathodic current (50 μA) for a given time, in order to obtain ca. five monolayers of coverage; the time for nickel plating was calculated according to the real surface area of the working electrode in order to deposit  $5 \times 726 \mu\text{C cm}^{-2}$ , with the latter value corresponding to the charge needed to deposit one monolayer of closely packed metallic nickel from a Ni<sup>II</sup> solution, assuming the

atomic radius of Ni to be 0.124 nm and a density of 8.908 g cm<sup>-3</sup>.<sup>30</sup>

All potentials in this work are reported versus the RHE. The potentials were converted to the RHE scale, according to eq 1:

$$E_{\text{RHE}} = E + E_{\text{ref}} + 0.059\Delta\text{pH} \quad (1)$$

where  $E_{\text{RHE}}$  is the potential on the RHE scale and  $E$  is the experimental potential measured with respect to the reference electrode potential ( $E_{\text{ref}}$ ).

For measurements in rigorously Fe-free NaOH electrolytes, we used a method reported by Boettcher et al.,<sup>13</sup> using a high-purity Ni(OH)<sub>2</sub> precipitate as an Fe absorbent to remove trace Fe from the NaOH electrolyte. Briefly, it consists of dissolving 99.999% pure Ni(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O in ultrapure water in a polypropylene tube. Next, 1.0 M NaOH was added to precipitate high-purity Ni(OH)<sub>2</sub>. The mixture was shaken and centrifuged, and the supernatant was decanted. The Ni(OH)<sub>2</sub> was washed three times by adding water and 1.0 M NaOH, redispersing the solid, centrifuging and decanting the supernatant. Finally, the tube was filled with 1.0 M NaOH for purification. The solid was redispersed and mechanically agitated for at least 10 min, followed by at least 3 h of resting. The mixture was centrifuged, and the purified NaOH supernatant was decanted into a polypropylene bottle for storage, and later used for the electrochemical experiments.

Prior to the electrochemical measurements, the working solution was deaerated with argon for 30 min and the cyclic voltammograms were collected at different scan rates (1.0, 10.0, and 50.0 mV s<sup>-1</sup>) with and without rotation. Afterward, the electrolyte was saturated with O<sub>2</sub> during 30 min and the same measurements were performed.

## ■ ASSOCIATED CONTENT

### Supporting Information

The Supporting Information is available free of charge on the ACS Publications website at DOI: 10.1021/acscatal.8b01447.

Cyclic voltammetry curves of platinum and nickel oxyhydroxide electrodes (PDF)

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### Notes

The authors declare no competing financial interest.

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